#### 1-100 GPM

Up to 150 PSI



**Model 3E** IMO Model 3E pumps are three screw, positive displacement, rotary pumps designed and engineered for excellent suction capability over a wide range of fluid viscosities. Flow rates (1 to 100 GPM) are proportional to rotating speed when the pump is operated within the recommended pressure range. The pump has the ability to self-prime in a piping system designed to facilitate this feature.

Pump

The unique IMO design—only three moving parts is the key to the model 3E pump performance. A precision bored housing encases the driven screw (power rotor) and intermeshing sealing screws (idler rotors). The accurately machined idler rotors conform perfectly to the threads of the power rotor and to the housing bores confining the fluid in a succession of closures or cavities. As the screws rotate, the fluid is moved axially from the inlet port to the outlet port in a continuous, uniform flow. This uniform axial flow results in a minimum of fluid pulsation and extremely quiet operation.

The rotating idler rotors generate a hydrodynamic film of fluid which supports the idlers in the housing bores and prohibits wearing contact. The strength of this film is based on fluid viscosity, pump pressure and speed. As pressure requirements increase, the hydrodynamic film can be strengthened by increasing viscosity or speed. Both the flow rate and pressure capability of the IMO pump increase with speed; thus higher speeds generally result in better performance and longer life.

The symmetrical arrangement of the rotors (screws) eliminates the need for bearings to absorb radial loads. Model 3E pumps contain only one ball bearing which positions the power rotor for proper operation of the mechanical seal. This permanently grease-packed bearing is isolated from the pumpage by the mechanical seal to prevent contamination and improper lubrication.

Model 3E pumps are offered in ten rotor sizes for foot or flange mounted configurations. A variety of construction materials are available to meet operating conditions and job specifications. Complete pump/ driver assemblies can be provided as required.

The simple compact design of the Model 3E pump permits fast, easy installation and low maintenance. The bearing and shaft seal are easily replaced when necessary. The pump can be positioned in 90 degree increments to accommodate piping arrangements. Periodic inspection can be made without removing the pump, and routine maintenance can be performed without distrubing system piping.

### Applications

Model 3E pumps are designed to meet the requirements for hydraulic, lubricating, seal, distillate, residual and fuel oil applications. These units have been widely utilized in such places as power plants, refineries, fuel oil burners, petrochemical plants, mechanical transmissions, and lubricating seal oil systems—wherever high performance and reliability in a compact design are required.

Typical applications are:

Lubrication of diesel engines, steam turbine/

generator sets, reciprocating and centrifugal compressors, transmission gears, large centrifugal pumps, high inlet pressure refrigeration screw compressors, and other rotating machinery.

**Circulation** of fuel oils, hydraulic oils, transformer insulating oil and most petroleum based fluids in general.

Transfer, loading and unloading of clean lube, fuel, waste and similar type oils in refineries, factories, storage or settling tanks and lube oil reservoirs.

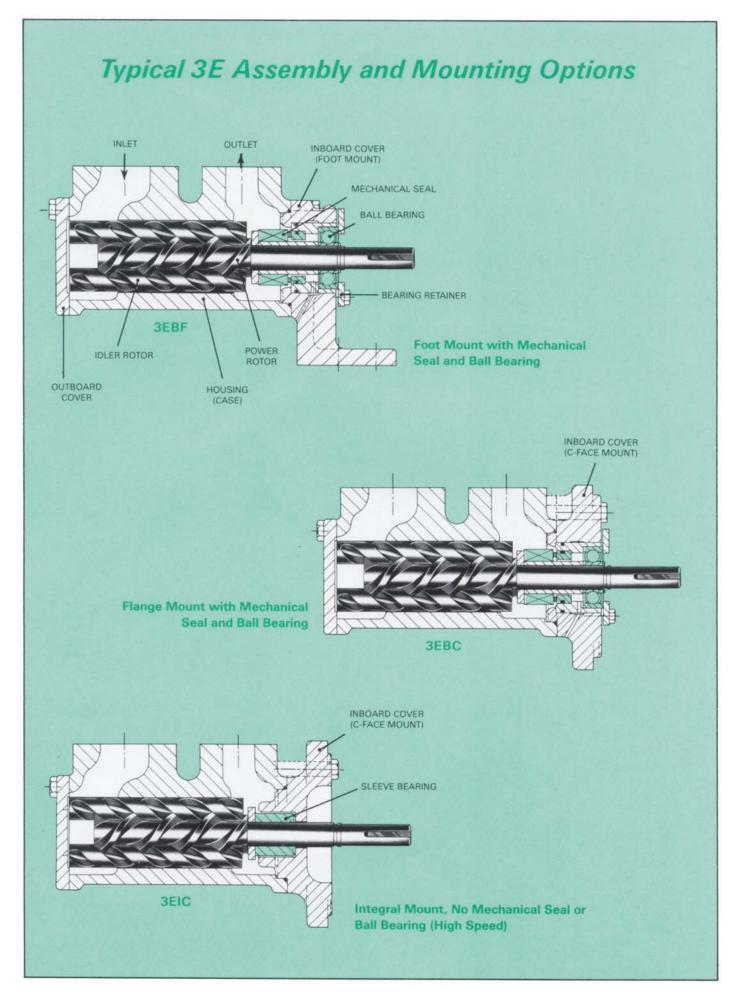
# Model 3E Specifications and Features

CASING	Pearlitic gray iron. Optional cast steel available in all sizes.
ROTOR HOUSING	Pearlitic gray iron. Replaceable in all cast steel models, and in $187 + 200$ size cast iron models.
POWER ROTOR	Alloy steel.
IDLER ROTORS	Pearlitic gray iron.
GASKETS	Cellulose and non-asbestos fiber.
PUMP INTERNALS	<ul> <li>Type B: (Sizes 87, 87P and 95) Positive drive mechanical seal, Buna-NO-rings and standard external permanently grease packed ball bearing. For all services up to 180°F and/or 25000 SSU.</li> <li>Type B: (Sizes 118-200) Buna-N bellows friction drive mechanical seal, Buna-NO-rings and</li> </ul>
	standard external permanently grease packed ball bearing. Recommended for distillate, lube oil and most lower viscosity, clean oil services in general.
	Type H: (Sizes 118-200) Positive drive mechanical seal, viton O-rings and external high temperature deep groove ball bearing. Recommended for residual oils and all applications with fluid viscosities above 2000 SSU
	applications with fluid viscosities above 3000 SSU. Type I: ( <u>All sizes</u> ) Integral flange mounted pump with sleeve bearing in lieu of a ball bearing and no shaft seal. For applications where pump shaft is within driving machinery enclosure, allowing internal return-to-sump of shaft leakage.
	Type N: ( <u>Available in C.I. case for flange mount—118-200 sizes only</u> ) Positive drive balanced mechanical seal, neoprene O-rings, carbon on carbide sealing faces and external grease packed deep groove ball bearing. For applications requiring higher inlet and discharge pressures.
DISCHARGE PRESSURE	150 PSIG maximum (Types B, H and I) 350 PSIG maximum (Type N, providing differential pressure does not exceed 150 psi.)
INLET PRESSURE	25 PSIG maximum (Types B, H and I) 300 PSIG maximum (Type N)
VISCOSITY	Type B and I: 33-3000 SSU (2.0-650 CST) Type H: 33-25000 SSU (2.0-5400 CST) Type N: 60-5000 SSU (10-1100 CST)
TEMPERATURE	Type B: 0-180°F Type H, I and N: 0-250°F, assuming fluid is within allowable viscosity limits.
DRIVE	Direct only.
ROTATION	Clockwise facing pump shaft. Optional countercloockwise available on all sizes, except Type N and 187M, 187Y.
MOUNTING	. May be foot or flange mounted in any attitude.
CONNECTIONS	All cast iron casing pumps and size 87P, 87 and 95 steel casing pumps are NPT connections. All other steel case pumps are SAE socket weld flanged (provided with pump).
FILTRATION	. Inlet strainers are required to keep contaminants and abrasives out of pump, but they must be selected by consultation with strainer vendor to prevent pump starvation. Normally, 60 mesh for light and 1/8"-3/16" openings for heavy oils are recommended.
ACCESSORIES	Pump/motor adapters for NEMA "C" face motors, steel bedplates and completely mounted pump/driver assemblies.

# Maximum Operating Speeds (RPM)\*

Size	87P, 87, 95	118P	118	143J	143	162	187,187Y,187M	200
Type B, H	5000	4000	4000	4000	4000	4000	4000	3800
Type N	3500	3500	3500	3500	3500	3500	3500	3500
Type I	8000	8000	6500	7000	5500	4800	4250	4000

\*Above values assume minimum suction conditions can be met.



# Model 3E Performance Data

	-	F	loto	Size	87	Р		
		-		d 3500				
Vis	cosity			ferentia		ure – I	PSI	
	ssu	25	50	75	100	125	150	
1	33	5.8	5.2	4.7	4.3	4.0	3.6	
ł	65	6.2	5.8	5.4	5.1	4.9	4.7	ure A)
	100	6.4	6.0	5.8	5.6	5.4	5.2	(PSIA)
5	150	6.6	6.3	6.0	5.9	5.7	5.6	t Pr
GPM	650	6.9	6.8	6.7	6.6	6.5	6.4	Inle
	1000	7.0	6.9	6.8	6.7	6.6	6.6	Net Inlet Pressure Required (PSIA)
	5000	7.1	7.1	7.0	7.0	7.0	6.9	2-
	10000	7.2	7.1	7.1	7.1	7.1	7.0	
	150	0.3	0.4	0.5	0.6	0.7	0.8	4.3
	650	0.6	0.7	0.8	1.0	1.1	1.2	4.4
ВНР	1000	0.8	0.9	1.0	1.1	1.2	1.3	4,5
B	5000	2.0	2.1	2.2	2.3	2.4	2.5	5.3
	10000	3.0	3.1	3.2	3.3	3.4	3.5	6.1
	10000	5.0	O.I	0.2	0.0			1.2310
			Spor	d 1750	RPM		-	
N/C					the state of the state of the		PSI	
	scosity SSU	25		fferenti			150	1.4
		25	50	75	100	125	150	
	33	2.2	0.1	-		-	-	ere (
	65	2.6	2.1	-	-			SIP
-	100	2.8	2.4	2.2	1.9	-	-	Net Inlet Pressure Required (PSIA)
GPM	150	2.9	2.6	2.4	2.2	2.1	1.9	let irec
0	650	3.3	3.2	3.0	3.0	2.9	2.8	t In
	1000	3.4	3.2	3.2	3.1	3.0	3.0	Ne
	5000	3.5	3.5	3.4	3.4	3.4	3.3	
	10000	3.5	3.5	3.5	3.5	3.4	3.4	
	150	0.1	0.2	0.2	0.3	0.3	0.4	3.7
4	650	0.2	0.2	0.3	0.3	0.4	0.5	3.8
внр	1000	0.2	0.3	0.3	0.4	0.4	0.5	3.9
	5000	0.5	0.6	0.6	0.7	0.7	0.8	4.0
	10000	0.8	0.8	0.9	0.9	1.0	1.0	4.2
			Spe	ed 115	ORPM		1.1	
Vi	scosity		D	ifferent	ial Pres	sure -	PSI	
	SSU	25	50	75	100	125	150	
	33	-	-	-		-	-	Ð
	65	1.3	-	-	-	-	-	sur (Al
	100	1.5	-	-	-	-	-	res
Σ	150	1.7	1.4	-	-	-	-	et P
GPM	650	2.0	1.9	1.8	1.7	1.6	1.6	Net Inlet Pressure Required (PSIA)
	1000	2.1	2.0	1.9	1.8	1.8	1.7	Vet
	5000	2.3	2.2	2.2	2.1	2.1	2.1	-
	10000	2.3	2.3	2.2	2.2	2.2	2.2	
	150	0.1	0.1		-	-	-	3.6
	650	0.1	0.1	0.2	0.2	0.2	0.3	3.6
внр	1000	0.1	0.1	0.2	0.2	0.3	0.3	3.6
8	5000	0.2	0.3	0.3	0.3	0.4	0.4	3.7
	10000	0.4	0.4	0.4	0.5	0.5	0.5	3.8

_		1		or Siz			2011 1 1 1 1	
M.	and its				A VIIV NO ANA	uro I	PSI	
	SSU	25	50	fferentia	100		150	1
		25		75		125	5.4	
	33	7.6	7.0	6.5	6.1	5.8		Đ.
	65	8.0	7.6	7.2	7.0	6.7	6.5 7.0	SIL
_	100	8.2	7.9	7.6	7.4	7.2	7.4	d (F
GPM	150	8.4	8.1	7.9	7.7	1942	CONTRACTO	Net Pressure Required (PSIA
0	650	8.7	8.6	8.5	8.4	8.3	8.2	Ne
	1000	8.8	8.7	8.6	8.5	8.5	8.4	ш
	5000	8.9	8.9	8.8	8.8	8.8	8.8	
-	10000	9.0	8.9	8.9	8.9	8.9	8.8	17
	150	0.3	0.5	0.6	0.7	0.9	1.0	4.7
٩	650	0.7	0.8	0.9	1.1	1.2	1.3	4.9
ВНР	1000	0.8	1.0	1.1	1.2	1.4	1.5	5.0
	5000	2.0	2.1	2.3	2.4	2.5	2.7	6.2
	10000	3.0	3.1	3.3	3.4	3.5	3.7	7.9
_		_	100		1.11.11.11.11.1			_
				ed 1750		_		_
Vi	scosity		-	ifferenti			PSI	
	SSU	25	50	75	100	125	150	
	33	3.1	2.4	-	-	-	-	e_
	65	3.5	3.0	2.7	2.4	-	-	SIA
	100	3.7	3.3	3.1	2.8	2.6	2.5	Net Inlet Pressure Required (PSIA)
GPM	150	3.8	3.6	3.3	3.1	3.0	2.8	et F
19	650	4.2	4.1	4.0	3.9	3.8	3.7	Inl
	1000	4.3	4.1	4.1	4.0	3.9	3.9	Net
	5000	4.4	4.4	4.3	4.3	4.3	4.2	
	10000	4.4	4.4	4.4	4.4	4.3	4.3	
	150	0.1	0.2	0.3	0.3	0.4	0.5	3.9
	650	0.2	0.3	0.3	0.4	0.5	0.5	4.0
внр	1000	0.2	0.3	0.4	0.4	0.5	0.6	4.1
-	5000	0.5	0.6	0.7	0.7	0.8	0.9	4.4
	10000	0.8	0.9	0.9	1.0	1.1	1.1	4.7
			Spe	ed 1150	RPM		1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	
V	iscosity		D	ifferent	ial Pres	sure -	PSI	
	SSU	25	50	75	100	125	150	
	33	1.5	-	-	-	-		
	65	1.9	1.5	-	-	-	1	A)
	100	2.1	1.8	1.5		-	-	ess
Σ	150	2.3	2.0	1.8	1.6	-	-	Net Inlet Pressure Required (PSIA)
GPM	650	2.6	2.5	2.4	2.3	2.2	2.2	nlet
	1000	2.7	2.6	2.5	2.4	2.4	2.3	et l
	5000	2.9	2.8	2.8	2.7	2.7	2.7	Z
	10000	2.9	2.9	2.8	2.8	2.8	2.8	1
	150	0.1	0.1	0.2	0.2	_	-	3.7
	650	0.1	0.1	0.2	0.2	0.3	0.3	3.7
внр	1000	0.1	0.2	0.2	0.2	0.3	0.3	3.8
8		0.1	0.2	0.2	0.3	0.4	0.5	3.9
	5000	0.5	0.5	0.5	0,4	0.4	0.5	5.5

10000 0.4

0.4

0.5

0.5

0.5

0.6

4.1

				or Si		5		_			
			1000	ed 350	1.5. Aut						
	scosity			ferenti				_			
-	SSU	25	50	75	100	125	150				
	33	9.9	9.1	8.6	8.1	7.7	7.3	e			
	65	10.3	9.8	9.4	9.1	8.8	8.6	SIA			
	100	10.6	10.2	9.9	9.6	9.4	9.1	Net Inlet Pressure Required (PSIA)			
GPM	150	10.8	10.4	10.2	10.0	9.8	9.6	et F red			
G	650	11.2	11.0	10.9	10.8	10.7	10.6	Inl			
	1000	11.3	11.1	11.0	11.0	10.9	10.8	Re			
	5000	11,4	11.4	11.3	11.3	11.3	11.2				
	10000	11.5	11.4	11.4	11.4	11.4	11.3				
	150	0.4	0.6	0.8	1.0	1.1	1.3	4.8			
	650	0.8	1.0	1.2	1.4	1.5	1.7	5.0			
BHP	1000	1.1	1.2	1.4	1.6	1.7	1.9	5.2			
	5000	2.6	2.7	2.9	3.1	3.2	3.4	6.8			
	10000	3.9	4.0	4.2	4.4	4.5	4.7	8.8			
			Spe	ed 175	0 RPM						
Vi	scosity	1	Di	fferenti	al Pres	sure –	PSI				
SSU 25 50 75 100 125 150											
	33	4.1	3.3	-	-	_					
	65	4.6	4.0	3.7	3.3	3.0		A)			
	100	4.8	4.4	4.1	3.8	3.6	3.4	esse			
5	150	5.0	4.6	4.4	4.2	4.0	3.8	Pr (I)			
GPM	650	5.4	5.2	5.1	5.0	4.9	4.8	nlet			
Ŭ	1000	5.5	5.3	5.2	5.2	5.1	5.0	Net Inlet Pressure Required (PSIA)			
	5000	5.7	5.6	5.5	5.5	5.5	5.4				
	10000	5.7	5.7	5.6	5.6	5.6	5.5				
	150	0.2	0.2	0.3	0.4	0.5	0.6	4.0			
	650	0.3	0.3	0.4	0.5	0.6	0.7	4.1			
đ	1000	0.3	0.4	0.4	0.6	0.6	0.7	4.1			
ВНР	5000	0.3	0.4	0.9	0.9	1.0	1.1	4.4			
			1.1	1.2	1.3	1.4	1.4	4.4			
_	10000	1.0	1.1	1.Z	1.3	1.4	1.4	4.8			
Live,			-								
		1		ed 115	Contraction of the		PSI				
VI	scosity SSU	25	1	fferent	1	1	1				
	1		50	75	100	125	150				
	33	2.1	-	-	-	-		e.			
	65	2.6	2.1	-		-	-	Net Inlet Pressure Required (PSIA)			
	100	2.8	2.4	2.1	-	-	-	Pre (P			
GPM	150	3.0	2.7	2.4	2.2	2.0	-	let			
9	650	3.4	3.3	3.1	3.0	2.9	2.8	t In			
	1000	3.5	3.4	3.3	3.2	3.1	3.0	Ne			
	5000	3.7	3.6	3.6	3.5	3.5	3.5				
	10000	3.7	3.7	3,6	3.6	3.6	3.6	-			
	150	0.1	0.1	0.2	0.3	0.3	-	3.7			
0	650	0.1	0.2	0.2	0.3	0.4	0.4	3.7			
внр	1000	0.2	0.2	0.3	0.3	0.4	0.4	3.8			
-	5000	0.3	0.4	0.4	0.5	0.5	0.6	3.9			
	10000	0.5	0.5	0.6	0.6	0.7	0.7	4.1			

### Rotor Size 118P

			Spe	ed 3500	RPM			
Vi	scosity		Di	fferentia	al Press	sure —	PSI	
	SSU	25	50	75	100	125	150	
6 11	33	15.4	14.3	13.4	12.7	12.0	11.5	
	65	16.2	15.4	14.8	14.2	13.8	13.4	IA)
	100	16.5	15.9	15.4	15.0	14.6	14.3	Pressure d (PSIA)
GPM	150	16.8	16.3	15.9	15.6	15.3	15.0	ed P
GF	650	17.5	17.2	17.0	16.9	16.7	16.6	Net Inlet F Required
	1000	17.6	17.4	17.2	17.1	17.0	16.9	Re
	5000	17.9	17.8	17.7	17.7	17.6	17.6	-
	10000	17.9	17.9	17.8	17.8	17.8	17.7	
	150	0.8	1.1	1.3	1.6	1.9	2.1	4,8
	650	1.6	1.9	2.1	2.4	2.6	2.9	5.0
BHP	1000	2.0	2.3	2.5	2.8	3.1	3.3	5.2
-	5000	5.0	5.2	5.5	5.7	6.0	6.3	6.8
	10000	7.5	7.7	8.0	8.3	8.5	8.8	8.8

			Spe	ed 175	0 RPM			
Vi	scosity		Di	fferenti	al Press	sure —	PSI	
	SSU	25	50	75	100	125	150	
	33	6.3	5.2	-	-	-	-	
	65	7.1	6.3	5.7	5.2	4.7	_	IA)
	100	7.5	6.8	6.4	5.9	5.6	5.2	Pressure d (PSIA)
Σ	150	7.8	7.3	6.8	6.5	6.2	5.9	ed P
GPM	650	8.4	8.2	8.0	7.8	7.7	7.6	Net Inlet F Required
	1000	8.6	8.4	8.2	8.1	7.9	7.8	Net Re
	5000	8.8	8.7	8.7	8.6	8.6	8.5	
1	10000	8.9	8.8	8.8	8.7	8.7	8.7	
	150	0.3	0.4	0.5	0.7	0.8	0.9	4.0
	650	0.5	0.6	0.7	0.9	1.0	1.1	4.1
внр	1000	0.6	0.7	0.8	1.0	1.1	1.2	4.1
-	5000	1.3	1.5	1.6	1.7	1.9	2.0	4.4
	10000	2.0	2.1	2.2	2.4	2.5	2.6	4.8

			Spe	ed 115	RPM			
Vi	scosity		Di	fferenti	al Press	sure –	PSI	
1	SSU	25	50	75	100	125	150	
	33	3.2	-	74	-	-		
	65	4.0	3.2		-			IA)
	100	4.4	3.7	3.3	-	-	-	ressure (PSIA)
Σ	150	4.7	4.2	3.7	3.4	3.1		a
GPM	650	5.3	5.1	4.9	4.7	4.6	4.5	Net Inlet I Required
	1000	5.5	5.3	5.1	5.0	4.8	4.7	Rec
	5000	5.7	5.6	5.6	5.5	5.5	5.4	2
	10000	5.8	5.7	5.7	5.6	5.6	5.6	
	150	0.1	0.2 .	0.3	0.4	0.5		3.7
	650	0.2	0.3	0.4	0.5	0.6	0.7	3.7
BHP	1000	0.3	0.4	0.5	0.5	0.6	0.7	3.8
-	5000	0.6	0.7	0.8	0.9	1.0	1.0	3.9
	10000	0.9	1.0	1.1	1.1	1.2	1.3	4.1

 For conditions between listed values, interpolate between those values. For conditions not listed or off tables, Contact IMO.
 Net Inlet Pressure Required is minimum pressure above vapor pressure at pump inlet to prevent cavitation. This assumes that the fluid is air and gas free.

3. For BHP values at viscosities below 150 SSU, use values listed for 150 SSU.

# Model 3E Performance Data

-		1	Roto	r Siz	e 11	8		
				d 3500				
Vis	cosity		Di	fferentia	al Press	sure —	PSI	
-	SSU	25	50	75	100	125	150	S. 16.
	33	19.9	18.8	17.9	17.2	16.6	16.0	
	65	20.7	19.9	19.3	18.8	18.3	17.9	IA)
	100	21.1	20.4	19.9	19.5	19.1	18.8	Pressur (PSIA
Σ	150	21.4	20.8	20.4	20.1	19.8	19.5	ed (
GPM	650	22.0	21.8	21.6	21.4	21.3	21.1	Inle
	1000	22.1	21.9	21.8	21.6	21.5	21.4	Net Inlet Pressure Required (PSIA)
	5000	22.4	22.3	22.2	22.2	22.1	22.1	2
	10000	22.5	22.4	22.4	22.3	22.3	22.2	
	150	0.9	1.2	1.5	1.9	2.2	2.5	5.4
	650	1.7	2.0	2.3	2.6	3.0	3.3	5.8
внр	1000	2.1	2.4	2.7	3.1	3.4	3.7	6.0
8	5000	5.0	5.3	5.7	6.0	6.3	6.7	8.8
	10000	7.5	7.9	8.2	8.5	8.8	9.2	14.7
			Spee	d 1750	RPM	6.1.1		
Vis	scosity		Di	fferenti	al Press	sure —	PSI	
	ssu	25	50	75	100	125	150	
	33	8.6	7.5	6.6	5.9	_	_	
	65	9.4	8.6	8.0	7.5	7.0	6.6	ure A)
	100	9.8	9.1	8.6	8.2	7.8	7.5	ess PSI
5	150	10.0	9.5	9.1	8.8	8.5	8.2	d (
GPM	650	10.7	10.4	10.3	10.1	9.9	9.8	Net Inlet Pressure Required (PSIA)
	1000	10.8	10.6	10.5	10.3	10.2	10.1	et l Req
	5000	11.1	11.0	10.9	10.9	10.8	10.8	Z.
	10000	11.2	11.1	11.0	11.0	11.0	10.9	
	150	0.3	0.5	0.6	0.8	1.0	1.1	4.1
	650	0.5	0.7	0.8	1.0	1.2	1.3	4.3
внр	1000	0.6	0.8	0.9	1.1	1.3	1.4	4.3
8	5000	1.4	1.5	1.7	1.9	2.0	2.2	4.9
	10000	2.0	2.2	2.3	2.5	2.7	2.8	5.6
			Spe	eed 115	0 RPN	1		
Vi	scosity			ifferent			PSI	
	SSU	25	50	75	100	125	150	
	33	4.7		-	-	-	_	1
	65	5.5	4.7	4.1	1	-	-	A)
	100	5.9	5.2	4.7	4.3	4.0		ess
Σ	150	6.2	5.6	5.2	4.9	4.6	4.3	t Pr
GPM	650	6.8	6.6	6.4	6.2	6.1	5.9	Inle
	1000	6.9	6.7	6.6	6.4	6.3	6.2	Net Inlet Pressure Required (PSIA)
	5000	7.2	7.1	7.1	7.0	6.9	6.9	24
	10000	7.3	7.2	7.2	7.1	7.1	7.1	
	150	0.2	0.3	0.4	0.5	0.6	0.7	3.8
	650	0.3	0.4	0.5	0.6	0.7	0.8	3.8
BHP	1000	0.3	0.4	0.5	0.6	0.7	0.8	3.9
B	5000	0.6	0.7	0.8	1.0	1.1	1.2	4.1
	10000	-	1.0	1.1	1.2	1.3	1.5	4.3
-	10000	0.0	1.0		1.16	1.0	1.0	1.0

		R	otor	Size	14:	3J		
			Spee	d 3500	RPM			
	scosity		Di	fferenti	al Press	sure –	PSI	
1	SSU	25	50	75	100	125	150	
1	33	26.9	25.5	24.5	23.6	22.9	22.2	0
	65	27.8	26.8	26.1	25.5	24.9	24.4	(AI)
	100	28.2	27.5	26.9	26.4	25.9	25.5	res (PS
GPM	150	28.6	27.9	27.5	27.1	26.7	26.4	Net Inlet Pressure Required (PSIA)
GF	650	29.4	29.1	28.8	28.6	28.5	28.3	Inle
	1000	29.5	29.3	29.1	28.9	28.8	28.7	Re
	5000	29.8	29.7	29.6	29.6	29.5	29.5	-
	10000	29.9	29.8	29.8	29.7	29.7	29.6	1
	150	1.4	1.8	2.3	2.7	3.1	3.6	5.2
	650	2.8	3.2	3.7	4.1	4.5	5.0	5.4
BHP	1000	3.5	4.0	4.4	4.8	5.3	5.7	5.7
	5000	8.8	9.2	9.6	10.1	10.5	11.0	7.8
	10000	13.2	13.6	14.1	14.5	15.0	15.4	11.5
			Spee	ed 1750	RPM			
Vi	scosity		Di	fferenti	al Pres	sure –	PSI	
	SSU	25	50	75	100	125	150	
	33	11.8	10.5	9.4	8,6	7.8	24	1
	65	12.7	11.8	11.1	10.4	9.9	9.4	IA)
	100	13.2	12.4	11.8	11.3	10.9	10.5	(PS
Σ	150	13.5	12.9	12.4	12.0	11.7	11.3	ed ed
GPM	650	14.3	14.0	13.8	13.6	13.4	13.3	Net Inlet Pressure Required (PSIA)
	1000	14.5	14.2	14.0	13.9	13.7	13.6	Net
	-	-						-

			. Marine	22201001	1. 1. 2 C - S	112,222		0
	65	12.7	11.8	11.1	10.4	9.9	9.4	(PSIA)
	100	13.2	12.4	11.8	11.3	10.9	10.5	res (PS
GPM	150	13.5	12.9	12.4	12.0	11.7	11.3	et P red
GP	650	14.3	14.0	13.8	13.6	13.4	13.3	Net Inlet Require
	1000	14.5	14.2	14.0	13.9	13.7	13.6	Net In Requ
	5000	14.8	14.7	14.6	14.5	14.5	14.4	
	10000	14.9	14.8	14.7	14.7	14.6	14.6	
	150	0.5	0.7	0.9	1.1	1.3	1.6	4.0
	650	0.8	1.0	1.3	1.5	1.7	1.9	4.1
ВНР	1000	1.0	1.2	1.4	1.7	1.9	2.1	4.2
	5000	2.3	2.6	2.8	3.0	3.2	3.4	4.6
	10000	3.5	3.7	3.9	4.1	4.3	4.6	5.2

			Spee	d 1150	RPM			
Vi	scosity		Dit	fferenti	al Press	sure —	PSI	
	SSU	25	50	75	100	125	150	
	33	6.6	5.3	-	-	-		
	65	7.6	6.6	5.9	5.3	-	-	ressure (PSIA)
	100	8.0	7.3	6.7	6.2	5.7	5.3	res (PS
GPM	150	8.4	7.7	7.3	6.9	6.5	6.2	Net Inlet P Required
GP	650	9.2	8.9	8.6	8.4	8.3	8.1	duit
	1000	9.3	9.1	8.9	8.7	8.6	8.4	Re
	5000	9.6	9.5	9,4	9.4	9.3	9.2	
	10000	9.7	9.6	9.6	9.5	9.5	9.4	
	150	0.2	0.4	0.5	0.7	0.8	1.0	3.7
	650	0.4	0.6	0.7	0.8	1.0	1.1	3.8
HP	dHg 1000	0.5	0.6	0.8	0.9	1.1	1.2	3.9
8	5000	1.1	1.2	1.4	1.5	1.6	1.8	4.0
	10000	1.6	1.7	1.9	2.0	2.1	2.3	4.2

Model 3E

				r Siz		0			
Vie	cosity			fferentia		uro - I			
	SSU	25	50	75	100	125	150		
	33	36.2	34.5	33.3	32.2	31.3	30.4	0	
-	65	37.3	36.1	35.2	34.5	33.8	33.2	sur SIA)	
	100	37.9	36.9	36.2	35.6	35.0	34.5	Pres (PS	
Visc S WdD	150	38.3	37.5	36.9	36.4	36.0	35.6	et F red	
9	650	39.2	38.9	38.6	38.3	38.1	37.9	Net Inlet Pressure Required (PSIA)	
	1000	39.4	39.1	38.9	38.7	38.5	38.4	Net	
	5000	39.8	39.7	39.6	39.5	39.4	39.3		
	150	1.5	2.1	2.7	3.3	3.9	4.5	6.2	
•	650	2.9	3.5	4.1	4.7	5.3	5.9	6.8	
H	1000	3.7	4.2	4.8	5.4	6.0	6.6	7.2	
-	5000	8.9	9.5	10.1	10.7	11.2	11.8	13.7	
-	5000	0.9	5.5	10.1	10.7	1.1.2	11.0	15.7	
			0	1 4750	0.044				
Mie	a a a la tra			ed 1750 fferenti			PSI	11	
	SSU	25	50	75	100	125	150		
_	33	16.1	14.5	13.2	12.1	11.2	10.3		
	65	100000000	16.1	15.2	14.4	13.7	13.1	A)	
	100	17.2	16.8	16.1	15.5	15.0	14.5	ess PSI	
GPM		18.2	17.4	16.8	16.3	15.9	14.5	Net Inlet Pressure Required (PSIA)	
PN	150			18.5	18.3	18.1	17.9	nlet	
0	650	19.2	18.8					et l Req	
	1000	19.3	19.0	18.8	18.6	18.5	18.3	Zu	
		0.0000000				19.3	19.3		
	The second second	Louis and the	-			19.6	19.5 2.0	4.3	
5000         19.7         19.6         19.5         19.4           10000         19.8         19.7         19.7         19.7         19.4           10000         19.8         19.7         19.7         19.7         19.4           150         0.5         0.8         1.1         1.4           650         0.9         1.2         1.5         1.4			1.7	2.4	4.4				
4	1000	1.1	1.4	1.7	2.0	2.2	2.4	4.4	
BHP	5000	2.4	2.7	3.0	3.3	3.6	3.9	5.3	
	10000	3.5	3.8	4.1	4.4	4.7	5.0	6.1	
	10000	3.0	3.0	4,1	4.4	4.7	5.0	0.1	
		-	Spe	eed 115	ORPN	1			
Vi	scosity			ifferent			PSI		
	SSU	25	50	75	100	125	150		
	33	9.2	7.6	-	-	-			
	65	10.4	9.2	8.3	7.5	6.9		A)	
	100	10.9	10.0	9.2	8.6	8.1	7.6	res	
Σ	150	11.3	10.6	10.0	9.5	9.0	8.6	ed P	
GPM	650	12.3	11.9	11.6	11.4	11.2	11.0	Net Inlet Pressure Required (PSIA)	
	1000	12.5	12.2	11.9	11.7	11.6	11.4	Rec	
	5000	12.9	12.7	12.6	12.5	12.5	12.4	2	
	10000	13.0	12.9	12.8	12.7	12.7	12.6		
	150	0.3	0.5	0.7	0.9	1.1	1.3	4.0	
	650	0.5	0.6	0.8	1.0	1.2	1.4	4.1	
BHP	1000	0.5	0.7	0.9	1.1	1.3	1.5	4.1	
B	5000	1.1	1.3	1.5	1.7	1.9	2.1	4.4	
				7 3 760					

		ŀ	Roto	r Siz	e 16	2		
			Spee	ed 3500	RPM			
Viscosity Differential Pressure – PSI								
5	SSU	25	50	75	100	125	150	
1	33	52.9	50.8	49.2	47.8	46.6	45.6	A)
	65	54.4	52.9	51.7	50.7	49.9	49.1	SSSI
	100	55.1	53.9	52.9	52.1	51.5	50.8	Pressure d (PSIA)
GPM	150	55.6	54.6	53.9	53.2	52.7	52.1	Net Inlet F Required
9	650	56.8	56.4	56.0	55.7	55.4	55.2	et lr lequ
	1000	57.1	56.7	56.4	56.1	55.9	55.7	ž"
	5000	57.6	57.4	57.3	57.1	57.1	57.0	
	150	2.2	3.1	3.9	4.8	5.6	6.4	7.0
٩	650	4.2	5.1	5.9	6.8	7.6	8.5	7.9
внр	1000	5.3	6.1	7.0	7.8	8.7	9.5	8.6
	2000	7.7	8.5	9.4	10.2	11.1	11.9	10.9
	5000	12.9	13.7	14.6	15.4	16.2	17.1	25.0

			Spee	ed 1750	RPM								
Vis	scosity		Differential Pressure — PSI										
:	SSU	25	50	75	100	125	150						
	33	23.9	21.8	20.2	18.8	17.6	16.6	0					
	65	25.4	23.9	22.7	21.8	20.9	20.1	ressure (PSIA)					
	100	26.1	24.9	23.9	23.2	22.5	21.9	Pres I (PS					
GPM	150	26.6	25.6	24.9	24.2	23.7	23.2						
GP	650	27.8	27.4	27.0	26.7	26.4	26.2	Net Inlet Require					
	1000	28.1	27.7	27.4	27.1	26.9	26.7	Re					
	5000	28.6	28.4	28.3	28.2	28.1	28.0						
	10000	28.7	28.6	28.5	28.4	28.3	28.3						
	150	0.8	1.2	1.6	2.0	2.5	2.9	4.4					
	650	1.3	1.7	2.1	2.6	3.0	3.4	4.6					
внр	1000	1.6	2.0	2.4	2.8	3.2	3.7	4.7					
	5000	3.5	3.9	4.3	4.7	5.2	5.6	5.7					
	10000	5.1	5.5	6.0	6.4	6.8	7.2	6.9					

			Spe	ed 1150	RPM	634					
Vis	scosity		D	Differential Pressure — PSI							
1	SSU	25	50	75	100	125	150				
	33	14.0	11.9	10.3	-	-		0			
	65	15.4	13.9	12.8	11.8	11.0	10.2	ressure (PSIA)			
1.5	100	16.1	14.9	14.0	13.2	12.5	11.9	res (PS			
GPM	150	16.7	15.7	14.9	14.3	13.7	13.2	Net Inlet P Required			
GF	650	17.9	17.4	17.1	16.8	16.5	16.2	Inl			
	1000	18.1	17.7	17.5	17.2	17.0	16.8	Net Re			
	5000	18.6	18.5	18.3	18.2	18.1	18.0				
	10000	18.8	18.6	18.5	18.5	18.4	18.3				
	150	0.4	0.7	1.0	1.3	1.5	1.8	4.0			
	650	0.7	0.9	1.2	1.5	1.8	2.0	4.1			
BHP	1000	0.8	1.0	1.3	1.6	1.9	2.2	4.2			
	5000	1.6	1.9	2.2	2.4	2.7	3.0	4.6			
the last	10000	2.3	2.6	2.9	3.2	3,4	3.7	5.2			

 For conditions between listed values, interpolate between those values. For conditions not listed or off tables, Contact IMO.
 Net Inlet Pressure Required is minimum pressure above vapor pressure at pump inlet to prevent cavitation. This assumes that the fluid is air and gas free

3. For BHP values at viscosities below 150 SSU, use values listed for 150 SSU

## Model 3E Performance Data

		R	otor	Size	187	/		
			Speed	3500	RPM			
Vi	scosity		Di	fferenti	al Pres	sure –	PSI	
	SSU	25	50	75	100	125	150	
	33	82.3	79.5	77.4	75.6	74.0	72.5	A Le
	65	84.2	82.3	80.7	79.4	78.3	77.3	Net Inlet Pressure Required (PSIA)
5	100	85.2	83.6	82.3	81.3	80.4	79.6	Pre
INI LO	150	85.9	84.6	83.6	82.7	82.0	81.3	lire
	650	87.5	86.9	86.4	86.0	85.7	85.3	equ
	1000	87.8	87.3	86.9	86.6	86.3	86.1	ž"
	2500	88.3	88.0	87.7	87.5	87.3	87.1	
	150	3.4	4.7	6.0	7.3	8.6	9.9	8.5
-	650	6.5	7.8	9.1	10.4	11.7	13.0	10.5
	1000	8.1	9.4	10.7	12.0	13.3	14.6	11.8
	1500	10.1	8.7	12.7	14.0	15.3	16.6	14.2
	2500	13.3	14.6	15.9	17.2	18.5	19.8	21.0
-		1	Speer	1750	RDM		-	
Vi	scosity			fferenti	11111111		PSI	
	SSU	25	50	75	100	125	150	
	33	37.8	35.0	32.8	31.0	29.4	28.0	
	65	39.7	37.7	36.2	34.9	33.8	32.7	A)
	100	40.6	39.0	37.8	36.8	35.9	35.0	SSSL SSSL
GPM	150	41.4	40.0	39.0	38.2	37.4	36.8	Net Inlet Pressure Required (PSIA)
	650	43.0	42.4	41.9	41.5	41.1	40.8	
	1000	43.3	42.8	42.4	42.1	41.8	41.5	equi
	5000	44.0	43.8	43.6	43.4	43.3	43.2	Ž"
	10000	44.1	44.0	43.9	43.8	43.7	43.6	
	150	1.2	1.8	2.5	3.1	3.8	4.4	4.8
	650	2.0	2.6	3.3	3.9	4.6	5.2	5.0
	1000	2.4	3.0	3.7	4.3	5.0	5.6	5.2
٥	5000	5.3	6.0	6.6	7.3	7.9	8.6	6.8
	10000	7.9	8.5	9.2	9.8	10.5	11.1	8.8
_								
11:				1150			DCI	
	scosity SSU	25		fferenti		-		-
-	1	25	50	75	100	125	150	
	33	22.5	19.7	17.6	15.8	10.5		e.
	65	24.5	22.5	20.9	19.6	18.5	17.5	SIA
	100	25.4	23.8	22.5	21.5	20.6	19.8	Net Inlet Pressure Required (PSIA)
	150	26.1	24.8	23.8	22.9	22.2	21.5	let
	650	27.7	27.1	26.6	26.2	25.9	25.5	t In
	1000	28.0	27.5	27.1	26.8	26.5	26.3	Ne
	5000	28.7	28.5	28.3	28.2	28.0	27.9	
-	10000	28.9	28.7	28.6	28.5	28.4	28.3	
	150	0.7	1.1	1.5	1.9	2.4	2.8	4.1
	650	1.0	1.4	1.9	2.3	2.7	3.1	4.3
5	1000 5000	1.2	1.6	2.0	2.5	2.9	3.3	4.3
	5000	2.5	2.9	3.3	3.8	4.2	4.6	4.9
	10000	3.6	4.0	4.4	4.9	5.3	5.7	5.6

		F	Roto	r Size	e 20	0	-		
			Speed	3500	RPM				
	scosity		Di	fferenti	al Press	sure –	PSI		
	SSU	25	50	75	100	125	150		
	33	100.4	97.2	94.8	94.8 92.7 90		89.3	A)	
	65	102.6	100.3	98.6	97.1	95.8	94.7	Net Inlet Pressure Required (PSIA)	
5	100	103.7	101.8	100.4	99.3	98.2	97.3	Pre	
GPM	150	104.5	103.0	101.8	100.9	100.0	99.3	Vet Inlet P Required	
0	650	106.3	105.6	105.1	104.6	104.2	103.8	t In equ	
	1000	106.7	106.1	105.7	105.3	105.0	104.7	Ne	
	1500	106.9	106.5	106.1	105.8	105.5	105.3	1	
	150	150 4.1		7.3	8.9	10.4	12.0	9.7	
P.	650	7.9	9.5	11.1	12.6	14.2	15.8	12.1	
BHP	1000	9.9	11.4	13.0	14.6	16.2	17.7	14.0	
	1500	12.2	13.8	15.4	17.0	18.5	20.1	18.0	
						-			
		1985	Speed	1750	RPM				
Vi	scosity		Di	ifferenti	al Press	sure —	PSI		
	SSU	25	50	75	100	125	150		
	33	46.4	43.2	40.7	38.7	36.9	35.2	1	
	65	48.6	46.3	44.6	43.1	41.8	40.6	IA)	
	100	49.6	47.8	46.4	45.2	44.2	43.2	resst (PSI)	
Σ	150	50.4	48.9	47.8	46.8	46.0	45.2	ed le	
GPM	650	52.3	51.6	51.0	50.6	50.2	49.8	Vet Inlet F Required	
	1000	52.6	52.1	51.6	51.2	50.9	50.6	Net Inlet Pressure Required (PSIA)	
	5000	53.4	53.2	53.0	52.8	52.6	52.5	-	
	10000	53.6	53.4	53.3	53.2	53.1	53.0		
	150	1.4	2.2	3.0	3.8	4.6	5.4	4.9	

			Speed	11150	RPM							
Vi	scosity		Differential Pressure — PSI									
	SSU	25	50	75	100	125	150					
	33	27.8	24.6	22.2	20.2	18.3						
	65	30.0	27.8	26.0	24.6	23.3	22.1	ressure (PSIA)				
	100	31.1	29.3	27.9	26.7	25.6	24.7	PS				
GPM	150	31.9	30.4	29.3	28.3	27.5	26.7	Net Inlet Pr Required (				
GF	650	33.8	33.1	32.5	32.1	31.6	31.3	Inle				
	1000	34.1	33.5	33.1	32.7	32.4	32.1	Red				
	5000	34.9	34.6	34.4	34.3	34.1	34.0	12				
	10000	35.1	34.9	34.7	34.6	34.5	34.4	1				
	150	0.8	1.3	1.8	2.4	2.9	3.4	4.2				
	650	1.2	1.7	2.3	2.8	3.3	3.8	4.4				
BHP	1000	1.4	2.0	2.5	3.0	3.5	4.0	4.5				
	5000	3.0	3.5	4.0	4.6	5.1	5.6	5.2				
	10000	4.3	4.9	5.4	5.9	6.4	6.9	5.9				

1 For conditions between listed values, interpolate between those values. For conditions not listed or off tables, Contact IMO.

2 Net Inlet Pressure Required is minimum pressure above vapor pressure at pump inlet to prevent cavitation. This assumes that the fluid is air and gas free.

650

1000

5000

10000

BHP

2.4

2.9

6.5

9.5

3.2

3.7

7.3

10.3

4.0

4.5

8.1

11.1

4.8

5.3

8.9

11.9

5.6

6.0

9.6

12.7

6.3

6.8

10.4

13.5

5.2

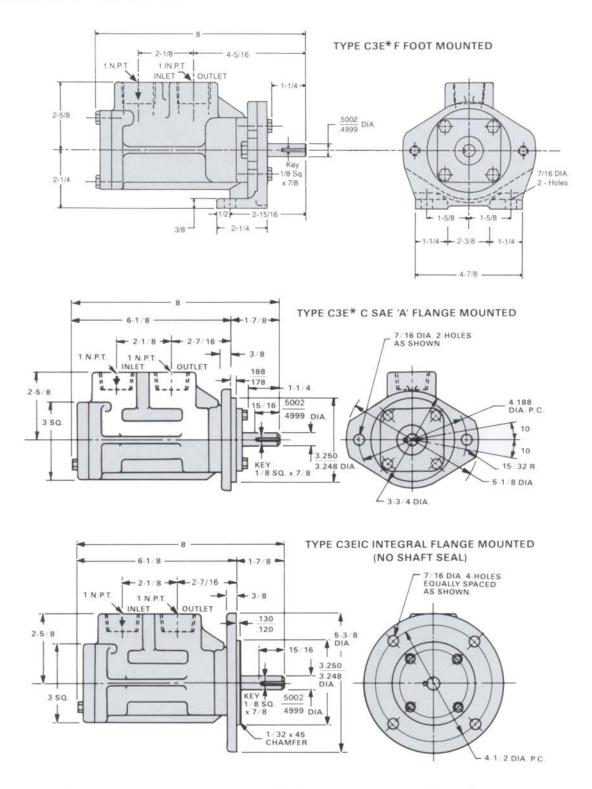
5.3

7.1

9.6

3 For BHP values at viscosities below 150 SSU, use values listed for 150 SSU.

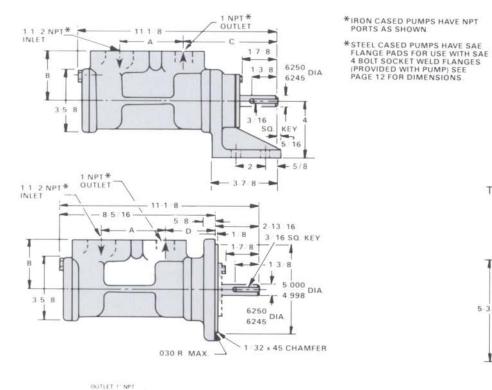
### Model 3E Dimensions Rotor Sizes 87P, 87 & 95



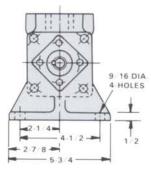


OFFICE	ROTATION	CASE MATERIAL	CERTIFIED BY	DATE
CUSTOMER			CUSTOMER ORDER	
MODEL NO			IMO ORDER	

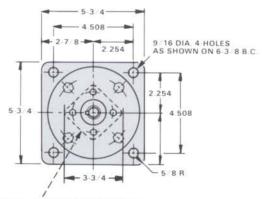
### Model 3E Dimensions Rotor Sizes 118P & 118



TYPE C3E \* F FOOT MOUNTED

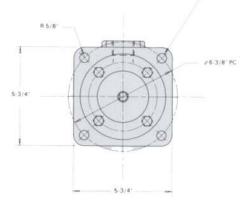


#### TYPES C3E\* "C" FLANGE MOUNTED



2-7/8" SQ x 1 / 4" THICK W/ 3/8" RADI-US CORNERS, FOR MECHANICAL SEAL MODEL (3E \* C) ONLY. NOT PRESENT ON INTEGRAL FLANGE MOUNT (3EIC) MODELS.





1

C3EIC-INTEGRAL FLANGE MOUNT-NO SEAL INCET 1.1/2 NPT 11 3/64" 5.5/16 1/8 = 2-7/16" --3/16 SQ KEY a 5 000 4 999 -15/8 1-3/8 p 6250 目 6245 R, 1/32 × 45

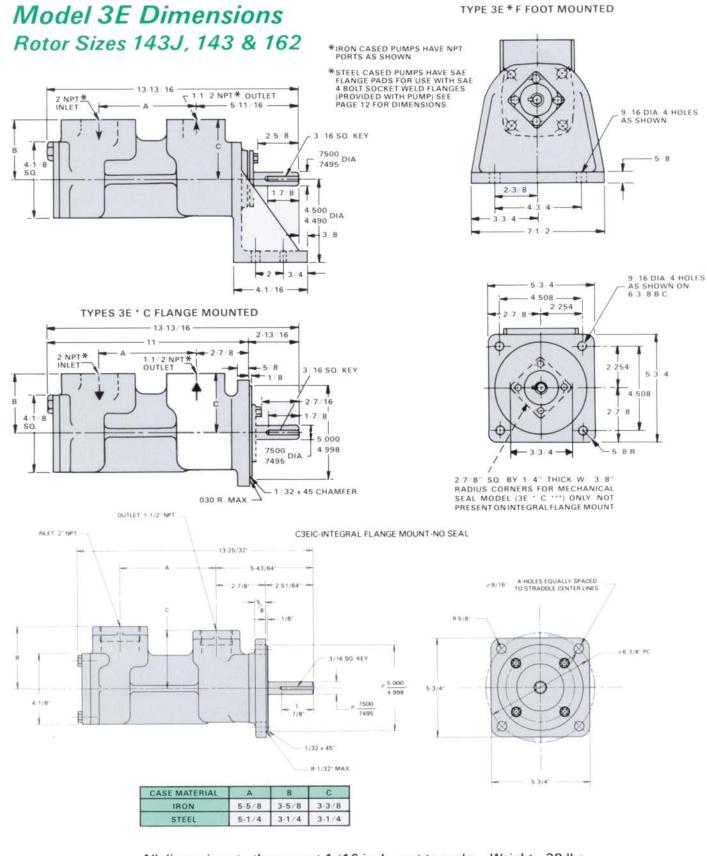
ATERIAL A B C

R 1/32 MAX

CASE MATERIAL	A	В	С	D
IRON	3-7/8	3-1/4	5-3/8	2-1/2
STEEL	3-1/2	2-3/4	5-1/4	2-3/8

#### All dimensions to the nearest 1/16 inch - not to scale. Weight - 27 lbs.

OFFICE	ROTATION     CASE MATERIAL     CERTIFIED BY       CW     CCW(D)     IRON     STEEL       CUSTOMER ORDER		CERTIFIED BY	DATE
CUSTOMER			CUSTOMER ORDER	
MODEL NO			IMO ORDER	



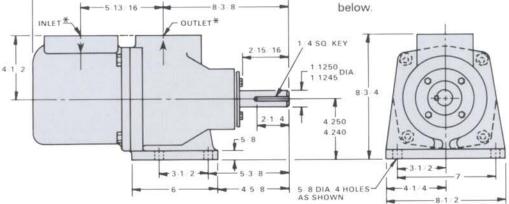


OFFICE	ROTATION	CASE MATERIAL	CERTIFIED BY	DATE
CUSTOMER			CUSTOMER ORDER	
MODEL NO			IMO ORDER	

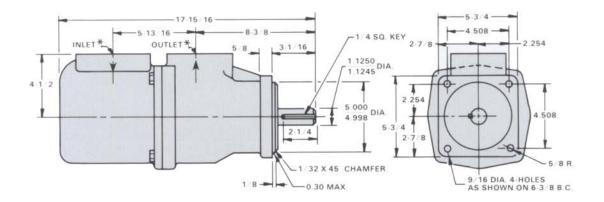
### Model 3E Dimensions Rotor Sizes 187 & 200

\*Iron Case Pumps have NPT ports. 2-1/2" Inlet - 2" Outlet.

\*Steel Case Pumps have SAE flange pads for use with SAE 4-bolt socket-weld flanges which are provided with the pump. 3" Inlet - 2" Outlet. See dimensions below.



17 15 16

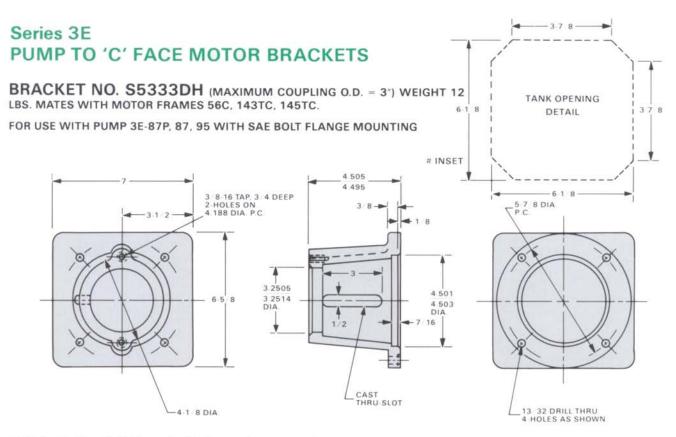


#### SAE 4-bolt socket-weld flanges (for steel case pumps 118 thru 200 sizes)

Part Number	Pipe Size	Pad Size	A	В	с	D	E	F	G Dia	H Dia	J Dia.	K Dia.
W4-16-16	1.00	1.00	2.31	2.75	1.031	2.062	.88	.25	1.328	1.00	1.560	.406
W4-24-24	1.50	1.50	3.25	3.69	1.406	2.750	1.19	.44	1.922	1.50	2.120	.531
W4-32-32	2.00	2.00	3.81	4.00	1.688	3.062	1.38	.50	2.406	2.00	2.495	.531
W4-48-48	3.00	3.00	5.16	5.31	2.438	4.188	2.12	.88	3.547	3.00	3.620	.656

All dimensions to the nearest 1/16 inch - not to scale. Weight - 92 lbs.

OFFICE	ICE ROTATION CASE MATERIAL CASE MATERIAL I RON I STEEL		CERTIFIED BY	DATE
CUSTOMER			CUSTOMER ORDER	
MODEL NO			IMO ORDER	



# This bracket is suitable for vertical tank mount arrangement. Drill 4 corner holes 7/16 dia. similar to brackets below. See inset of tank cover hole size.

#### FOR USE WITH PUMP 3E-118P, 118, 143J, 143, 162, 187, 200 WITH SAE 4 BOLT FLANGE MOUNTING

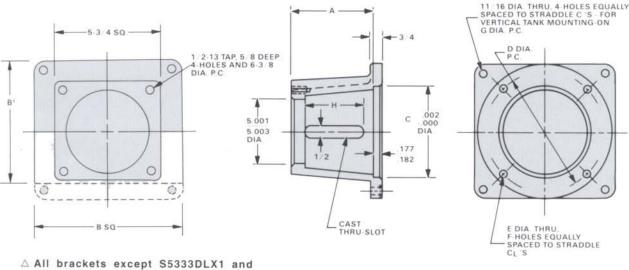
	PUMP		WHER	USED									1		
MOTOR FRAMES	AOTOR SIZES	BRACKET	HORIZONTAL	TANK TOP	A		81	c	D	E	F	α	н	JA	Ibs.
:50C-145C	118 to 200	\$53330L		x	6-3/16	9	-	4.501	5-7/8	7/16	4	11-1/4	3-1/2	8-1/4	23
	118 to 200	\$5333DLX1	×		6-3/16	9	7-15/16	4.501	5-7/8	7/16	4	-	3-1/2	-	22
182TC-184TC	118 to 162	\$5333DP	x	-	0	8-7/8**	-	8.501	7-1/4	9/16	.4		3-7/8	-	19
182TC-256TC	118 to 200	\$5333DJ		×	7-7/16	9	-	8.501	7-1/4	9/16	4	11-1/4	4	8-3/8	22
213TC-256TC	187 to 200		×		7-7/18	9	-	8.501	7-1/4	9/16	4	11-1/4	4	-	22
BATSC-365TSC	118 to 200	85333DK	x	x	7-5/18	14		12.501	11	11/16	8	16	4	13	37

0

0

0

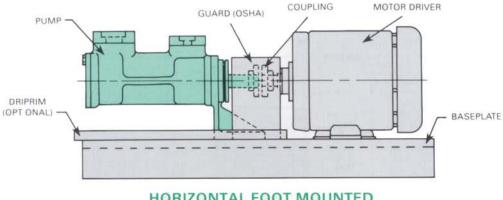
\*284TSC and 286TSC motors must have large (12  $\cdot$  1/2') 'AK' diam \*\*Supplied with a Round Flange



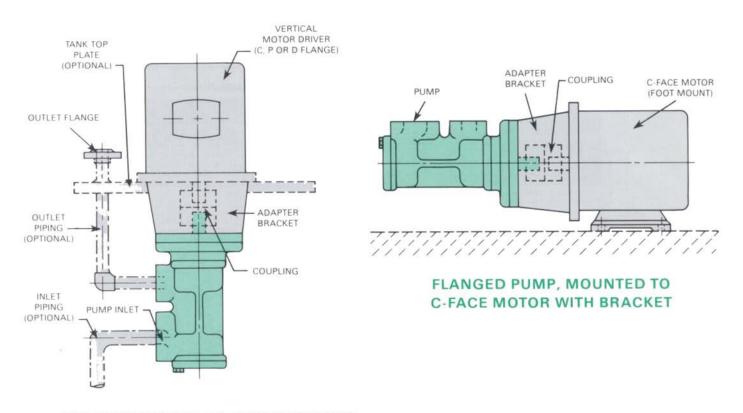
S5333DP, are suitable for vertical tank mount arrangement. Hole diameter in tank cover to mount bracket should be "J".

MATERIAL: ASTM A48, CL.40B CAST IRON, DIMENSIONS IN INCHES NOT TO SCALE. MAXIMUM COUPLING O.D. 4-3/4". SELECT FLEXIBLE COUPLING TO ACCOMMODATE: MAXIMUM COUPLING O.D., MOTOR TORQUE, SHAFT TO SHAFT GAP AND PUMP AND MOTOR SHAFT DIAMETERS.

## Typical 3E Pump/Motor Arrangements





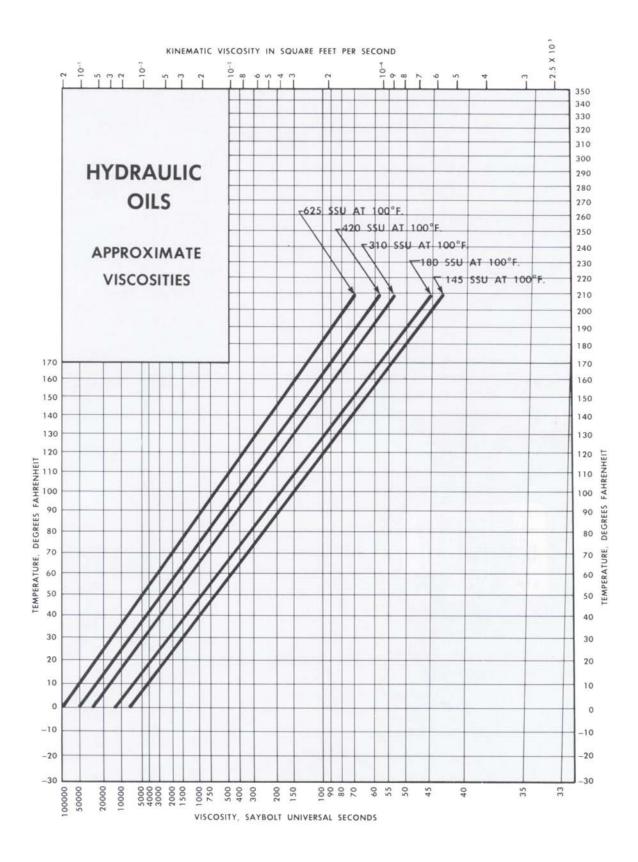


#### VERTICALLY IN-TANK MOUNTED WITH **OPTIONAL DISCHARGE PIPING AND TANKPLATE**

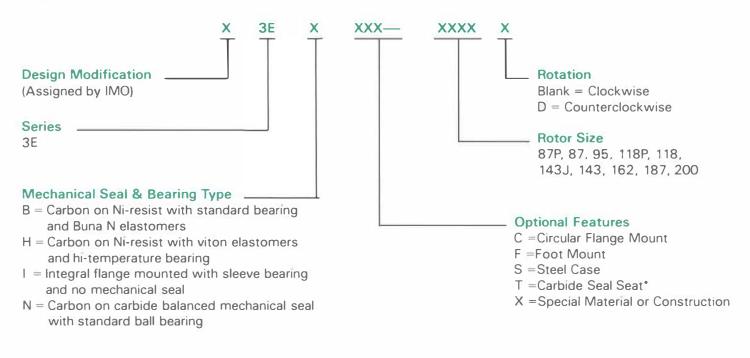
#### NOTES:

- 1. Pump/motor assemblies with OSHA type coupling guard and shaft coupling, factory mounted on a steel baseplate (with or without driprim) are available upon request.
- 2. Factory mounted pump/motor assemblies, complete with bracket, shaft coupling plus optional mounting plate, inlet (suction) and outlet (discharge) piping are available upon request.
- 3. For arrangements or variations not shown, consult IMO.

## Effect of Temperature on Hydraulic Oil Viscosity



## **Typical 3E Nomenclature**



#### Examples:

C3EBC-187 C3EHFS-143 Model 3E with standard seal and bearing, flange mounted, cast iron casing with 187 rotor size. Model 3E with positive drive mechanical seal (standard faces), high temperature bearing, foot mounted, steel casing with 143 rotor size.

\*Consult IMO for optional mechanical seal materials.



Quality Management System











### FOR MORE INFORMATION CONTACT:



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